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# Second-moment closure for turbulent scalar transport at various Prandtl numbers

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**Abstract**—A new second-moment closure model for turbulent scalar transport is proposed on the basis of the correlation coefficients between the flow variables and their derivatives that appear in the scalar-pressure gradient and dissipation terms of a turbulent scalar flux. Since these correlation coefficients should respond sensitively to a change in any of the time scales characteristic of turbulent transport, the model is given as a function of their ratios, which can be written in terms of turbulent Reynolds number, ( $Re_t = k^2/\nu\epsilon$ ), Prandtl number ( $Pr = \nu/\alpha$ ) and time scale ratio ( $R = (k_0/\epsilon_0)/(k/\epsilon)$ ). The conventional modeling methodology, i.e. the high Reynolds number hypothesis is abandoned, although the proposed model asymptotes to the well-established model expression in high Reynolds/Peclet number flows. As a result, the scalar fluxes are predicted very well in the homogeneous as well as wall-shear flows over a wide Prandtl number range. Copyright © 1996 Elsevier Science Ltd

## 1. INTRODUCTION

A mathematical model of turbulent scalar transport is required for solving the Reynolds-averaged scalar equation. With the recent advances in computers, the popularity of second-moment closure, at least in the research community, has considerably increased, though the turbulent Prandtl number models are still in wide use in engineering applications. In the second-moment closure, the generation terms due to mean velocity and scalar gradients can be handled exactly, and this feature should be one of the most attractive advantages when predicting complex flows. In recent years, various mathematical and/or physical constraints such as rapid distortion theory [1], realizability [2] and frame indifference [3] have been taken into account in modeling each of the generating and destruction processes in order to obtain a model of wide applicability; this can only be done for the model of this level. Current efforts are directed toward developing new models, especially of the pressure-scalar gradient correlation term to improve the overall accuracy of existing models [4, 5]. Although the developed models demonstrated improvements in thin shear flows, they sometimes gave poor predictions compared to those obtained by the previous models in more general cases [6, 7]. Besides, an introduction of such additional constraints as those mentioned above has resulted in very complex model structures, which may not be desirable for engineering calculations. There has been even an attempt to inten-

tionally abandon some of the constraints in order to possess a simpler and well-balanced model expression [8].

In scalar flux modeling, the major weakness lies in the fact that most of the scalar field models are developed in the same modeling procedure as the velocity field models. Therefore, they are basically applicable only for gaseous flows at  $Pr \approx 1$  and their physical basis is questionable when the Prandtl number is far from unity. For predicting various Prandtl number fluid flows, several turbulent Prandtl number models [9–11] and scalar field two-equation models [12] can be found in the literature, but only a few second-moment closures have been proposed so far [13, 14]. A difficulty exists in the choice of the relevant time scales that are indispensable to modeling unknown correlations between velocity and scalar fluctuations. For instance, even for a simple scalar field, it is not physically clear which time scale,  $k/\epsilon$  or  $k_0/\epsilon_0$ , should be adopted, and the selection will be even more ambiguous in low Peclet number flows with additional time scales such as  $\sqrt{\alpha/\epsilon}$ . It is impossible, however, to incorporate these effects into the model only from a dimensional argument. Hence, a new approach must be introduced. Furthermore, it is known that the scalar-pressure gradient correlation term is not generally aligned with either the scalar flux vector or the mean scalar gradient vector; one can expect a serious difficulty in deriving a simple relationship among these vectors. This is actually the case in strongly sheared turbulence, where the ratio of the streamwise to cross-stream scalar flux components is considerably large ( $-\bar{u}_1\theta/\bar{u}_2\theta > 2$ ), whereas that of the scalar-pressure gradient correlation term remains moderate [5, 15].

From the viewpoints above, we presently construct

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## NOMENCLATURE

$a_{ij}$	stress anisotropy, $\overline{u_i u_j} / k - 2/3 \delta_{ij}$	$U_i, u_i$	mean and fluctuating velocity components
$A$	flatness parameter, $1 - 9/8(A_2 - A_3)$	$V_{i\theta}$	molecular diffusion term of turbulent scalar flux, in equation (1)
$A_2$	second invariant of stress anisotropy, $a_{ij} a_{ij}$	$x_i$	$i$ th coordinate.
$A_3$	third invariant of stress anisotropy, $a_{ij} a_{jk} a_{ki}$		
$f_{\varepsilon 1}, f_{\varepsilon 2}$	functions in $\varepsilon_{i\theta}$ model, equation (12)		
$f_{\Pi 1}, f_{\Pi 2}$	functions in $\Pi_{i\theta}$ model, equation (11)		
$f_w$	weighting function in the near-wall region, equations (50), (51) and (52)		
$k$	turbulent kinetic energy, $\overline{u_i u_i} / 2$		
$k_\theta$	scalar variance, $\overline{\theta^2} / 2$		
$Nu$	Nusselt number		
$P$	production of turbulent kinetic energy		
$Pr$	Prandtl number, $\nu / \alpha$		
$Pr_t$	turbulent Prandtl number		
$P_{i\theta}, P_\theta$	production terms of turbulent scalar flux and scalar variance, in equations (1) and (37)		
$R$	time scale ratio, $(k_\theta / \varepsilon_\theta) / (k / \varepsilon)$		
$Re_t$	turbulent Reynolds number, $k^2 / \nu \varepsilon$		
$S$	mean velocity gradient, $\partial U_1 / \partial x_2$		
$t$	time		
$T_{i\theta}, T_\theta, T_{\varepsilon\theta}$	turbulent diffusion terms of turbulent scalar flux, scalar variance and its dissipation rate, in equations (1), (37) and (39)		
		Greek symbols	
		$\alpha$	thermal diffusivity
		$\varepsilon, \varepsilon_\theta$	dissipation terms of $k$ and $k_\theta$
		$\varepsilon_{i\theta}$	dissipation term of turbulent scalar flux, in equation (1)
		$\Theta, \theta$	mean and fluctuating scalar
		$\lambda$	Taylor microscale, $\sqrt{(10\nu k / \varepsilon)}$
		$\lambda_\theta$	scalar Taylor microscale, $\sqrt{(12\alpha k_\theta / \varepsilon_\theta)}$
		$\nu$	kinematic viscosity
		$\Pi_{i\theta}$	scalar-pressure gradient correlation term, in equation (1)
		$\rho$	density
		$\phi_{i\theta}$	pressure-scalar gradient correlation term, in equation (2).
		Subscripts and superscripts	
		$( ), i$	partial derivative with respect to $x_i$
		$( )$	ensemble average
		$( )'$	root-mean-square value.

a second-moment closure that can be applied to flows of a wide Reynolds and Prandtl number range. In other words, the dependence of the model on the turbulent Reynolds number  $Re_t$ , the molecular Prandtl number  $Pr$  and the time scale ratio  $R$  is properly accounted for. This cannot be done from a dimensional analysis alone, and in the present study, we pay special attention to the correlation coefficients between unknown variables, since they are greatly affected by the parameters mentioned above [16].

The following section describes the derivation of a second closure for handling multiple time scale problem of turbulence. Then, the model is tested and evaluated in several homogeneous flows and in fully-developed channel flows at various Prandtl and Reynolds numbers.

## 2. MODEL DEVELOPMENT

### 2.1. Modeling $\Pi_{i\theta}$ and $\varepsilon_{i\theta}$

When any buoyancy effect can be neglected, the transport equation for the scalar flux in a fluid of constant physical properties is given as :

$$\frac{D\overline{u_i \theta}}{Dt} = \underbrace{-\overline{u_i u_k} \frac{\partial \Theta}{\partial x_k}}_{P_{i\theta}} - \underbrace{u_k \theta \frac{\partial U_i}{\partial x_k}}_{\Pi_{i\theta}} - \underbrace{\frac{1}{\rho} \theta \frac{\partial p}{\partial x_i}}_{\Pi_{i\theta}} - \underbrace{(\alpha + \nu) \frac{\partial \theta}{\partial x_k} \frac{\partial u_i}{\partial x_k}}_{\varepsilon_{i\theta}} - \underbrace{\frac{\partial}{\partial x_k} \overline{u_i u_k \theta}}_{T_{i\theta}} + \underbrace{\frac{\partial}{\partial x_k} \left( \alpha u_i \frac{\partial \theta}{\partial x_k} + \nu \theta \frac{\partial u_i}{\partial x_k} \right)}_{V_{i\theta}}. \quad (1)$$

The scalar-pressure gradient correlation term  $\Pi_{i\theta}$  and the dissipation term  $\varepsilon_{i\theta}$  are major sink terms and need to be carefully modeled. In conventional turbulence modeling,  $\Pi_{i\theta}$  has been divided into the pressure-scalar gradient correlation term  $\phi_{i\theta}$  and the pressure diffusion term; the latter has been usually ignored or thought of as being absorbed into the turbulent diffusion term :

$$-\frac{1}{\rho} \theta \frac{\partial p}{\partial x_i} = \underbrace{\frac{1}{\rho} p \frac{\partial \theta}{\partial x_i}}_{\phi_{i\theta}} - \underbrace{\frac{1}{\rho} \frac{\partial p \theta}{\partial x_i}}_{\text{pressure diff.}}. \quad (2)$$

The dissipation term has been assumed to be isotropic ( $\varepsilon_{i\theta} = 0$ ) and the effect of anisotropic dissipation has been expressed implicitly within the model of  $\phi_{i\theta}$ . This reduces the problem to the modeling of  $\phi_{i\theta}$  alone, and one of the simplest model for  $\phi_{i\theta}$  is written as [17] (Basic model, hereafter) :

$$\phi_{i\theta} = -3.0 \frac{\varepsilon}{k} \overline{u_i \theta} + 0.5 \overline{u_k \theta} \frac{\partial U_i}{\partial x_k}. \quad (3)$$

However, there are some situations where this approach seems inappropriate, e.g. in low Peclet number flows  $\varepsilon_{i\theta}$  dominates the flux destruction mechanism. Since  $\Pi_{i\theta}$  and  $\varepsilon_{i\theta}$  represent physically distinct mechanisms, they are modeled separately in this study.

We define the correlation coefficients of  $\Pi_{i\theta}$  and  $\varepsilon_{i\theta}$ , respectively, as follows :

$$\begin{aligned} & -\frac{1}{\rho} \overline{\theta \frac{\partial p}{\partial x_i}} \left/ \left[ \frac{1}{\rho} \sqrt{\overline{(\theta^2)}} \sqrt{\overline{\left( \left( \frac{\partial p}{\partial x_{(i)} \right)^2 \right)}}} \right] \right. \quad (4) \\ (v+\alpha) \frac{\partial u_i}{\partial x_j} \frac{\partial \theta}{\partial x_j} \left/ \right. & \\ \left[ (v+\alpha) \sqrt{\overline{\left( \left( \frac{\partial u_{(i)}}{\partial x_k} \right)^2 \right)}} \sqrt{\overline{\left( \left( \frac{\partial \theta}{\partial x_i} \right)^2 \right)}} \right] & \quad (5) \end{aligned}$$

where the indices in parentheses do not obey the summation convention rule. If the two fluctuating components, i.e.  $\theta$  and  $\partial p/\partial x_i$ , or  $\partial u_i/\partial x_k$  and  $\partial \theta/\partial x_k$ , are well correlated, the above coefficients should be of the order of one. However, the correlations between those components are generally poor, because they are associated with different scales. For example, fluctuations such as  $u$  and  $\theta$  are tuned to low wave numbers, whereas  $\partial p/\partial x_i$ ,  $\partial u_i/\partial x_j$  and  $\partial \theta/\partial x_i$  are the spacial derivatives of fluctuating quantities that become large at high wave numbers. With these facts, the modeling of  $\Pi_{i\theta}$  and  $\varepsilon_{i\theta}$  should be especially difficult. For example, the correlation between velocity–scalar fluctuations at low wave numbers and scalar–velocity fluctuations at high wave numbers is hard to parameterize. Besides, when Prandtl number is apart from unity, the velocity and scalar scales characteristic of high wave numbers become much different, because viscous and molecular diffusivities affect the velocity and scalar fields differently.

In this study, we assume that dimensionless form of  $\Pi_{i\theta}$  can be generally related to functions of the scalar flux and its production terms as :

$$\begin{aligned} & \frac{-\frac{1}{\rho} \overline{\theta \frac{\partial p}{\partial x_i}}}{\frac{1}{\rho} \sqrt{\overline{(\theta^2)}} \sqrt{\overline{\left( \left( \frac{\partial p}{\partial x_{(i)} \right)^2 \right)}}} = \text{func.} \left( \frac{\overline{u_i \theta}}{\sqrt{\overline{(u_{(i)}^2)}} \sqrt{\overline{(\theta^2)}}}, \right. \\ & \left. \frac{-\overline{u_i u_j} \frac{\partial \Theta}{\partial x_j}}{P \sqrt{\overline{(k_\theta/k)}}}, \frac{-\overline{u_j \theta} \frac{\partial U_i}{\partial x_k}}{P \sqrt{\overline{(k_\theta/k)}}}, \dots \right). \quad (6) \end{aligned}$$

Since the above equation simply shows the relation between the anisotropy of dimensionless variables, we retain only the correlation coefficient of the scalar flux in the right-hand side of equation (6) for the first-order approximation. The effect of mean velocity gradient on fluctuating pressure will be expressed implicitly through  $P/\varepsilon$  in the model of  $\sqrt{\overline{(p^2)}}$  [see equation (28)]. If we further assume that the correlation coefficient of  $\varepsilon_{i\theta}$  should be also a function of that of the scalar flux, we have :

$$\frac{\Pi_{i\theta}}{\frac{1}{\rho} \sqrt{\overline{(\theta^2)}} \sqrt{\overline{\left( \left( \frac{\partial p}{\partial x_{(i)} \right)^2 \right)}}} = C_\Pi f_{\Pi 1} f_{\Pi 2} \frac{\overline{u_i \theta}}{\sqrt{\overline{(u_{(i)}^2)}} \sqrt{\overline{(\theta^2)}}} \quad (7)$$

$$\begin{aligned} & \frac{\varepsilon_{i\theta}}{(v+\alpha) \sqrt{\overline{\left( \left( \frac{\partial u_{(i)}}{\partial x_k} \right)^2 \right)}} \sqrt{\overline{\left( \left( \frac{\partial \theta}{\partial x_i} \right)^2 \right)}}} \\ & = C_\varepsilon f_{\varepsilon 1} f_{\varepsilon 2} \frac{\overline{u_i \theta}}{\sqrt{\overline{(u_{(i)}^2)}} \sqrt{\overline{(\theta^2)}}} \quad (8) \end{aligned}$$

where

$$0 \leq f_{\Pi 1}, f_{\Pi 2}, f_{\varepsilon 1}, f_{\varepsilon 2} \leq 1.$$

Note that the coefficients  $C_\Pi$  and  $C_\varepsilon$  should be of  $O(1)$  and that the functions  $f_{\Pi 1}$ ,  $f_{\Pi 2}$ ,  $f_{\varepsilon 1}$  and  $f_{\varepsilon 2}$  vary from unity to zero in order to express the decrease in the correlation coefficients of  $\Pi_{i\theta}$  and  $\varepsilon_{i\theta}$ . Functions  $f_{\Pi 1}$  and  $f_{\varepsilon 1}$  stand for the effect of scale difference between large and fine motions. On the other hand, functions  $f_{\Pi 2}$  and  $f_{\varepsilon 2}$  represent the effect of scale difference between scalar and velocity fluctuations at high wave numbers. Note that each side of these equations will not take a value much far from unity, but this constraint has not been taken into account in the previous models.

Equations (7) and (8) contain variables such as the derivative of fluctuating pressure, which should require further modeling. The pressure fluctuation is related to the turbulent kinetic energy as  $\sqrt{\overline{(p^2)}} = C_p \rho k$ . For the pressure derivative tensor  $\overline{p_i p_j}$ , the following two candidate expressions are adopted as a first-order approximation :

$$\frac{1}{\rho^2} \overline{\frac{\partial p}{\partial x_i} \frac{\partial p}{\partial x_j}} \sim \frac{1}{3} \frac{1}{\rho^2} \overline{\frac{\partial p}{\partial x_k} \frac{\partial p}{\partial x_k}} \delta_{ij} \sim C_p^2 \frac{k^2}{\lambda^2} \delta_{ij} \quad (9)$$

$$\frac{1}{\rho^2} \overline{\frac{\partial p}{\partial x_i} \frac{\partial p}{\partial x_j}} \sim \frac{1}{\rho^2} \overline{\frac{\partial p}{\partial x_k} \frac{\partial p}{\partial x_k} \frac{u_i u_j}{2k}} \sim C_p^2 \frac{k^2}{\lambda^2} \frac{\overline{u_i u_j}}{k} \quad (10)$$

where  $\lambda$  is the Taylor microscale. With these estimates introduced into equation (7), we have two general models for the scalar–pressure gradient correlation term as :

$$\Pi_{i\theta} = \begin{cases} C_{\Pi} f_{\Pi 1} f_{\Pi 2} C_p \sqrt{(Re_t)} \sqrt{\left(\frac{k}{2\overline{u_{i0}^2}}\right) \frac{\varepsilon}{k} \overline{u_i \theta}} & \text{(Model 1)} \\ \frac{\sqrt{3}}{2} C_{\Pi} f_{\Pi 1} f_{\Pi 2} C_p \sqrt{(Re_t)} \frac{\varepsilon}{k} \overline{u_i \theta} & \text{(Model 2).} \end{cases} \quad (11)$$

The coefficient  $\sqrt{3}/2$  is introduced so that Models 1 and 2 give exactly the same form in isotropic turbulence. If we also assume  $\overline{u_{i,k} u_{j,k}}/\varepsilon = \overline{u_i u_j}/2k$  in low Reynolds number flows, where  $\varepsilon_{i0}$  is important, equation (8) can be rewritten as:

$$\varepsilon_{i0} = C_r f_{\varepsilon 1} f_{\varepsilon 2} \frac{1 + Pr}{2\sqrt{(Pr)}\sqrt{(R)}} \frac{\varepsilon}{k} \overline{u_i \theta}. \quad (12)$$

These equations do not satisfy some modeling constraints, i.e. vectorial invariance (Model 1), realizability [18] and linear property of scalar equations [19]. In the following, each of the model functions  $f_{\Pi 1}$ ,  $f_{\Pi 2}$ ,  $f_{\varepsilon 1}$  and  $f_{\varepsilon 2}$  is determined.

As mentioned earlier, the scalar-pressure gradient correlation term  $\Pi_{i\theta}$  can be written as a sum of the pressure-scalar gradient correlation term  $\phi_{i\theta}$  and the pressure diffusion term. In most practical flows and far from a wall, the pressure diffusion term is relatively small, and the following relation should be a good approximation:

$$\underbrace{-\frac{1}{\rho} \frac{\partial p}{\partial x_i}}_{\Pi_{i\theta}} = \underbrace{\frac{1}{\rho} \frac{\partial \theta}{\partial x_i}}_{\phi_{i\theta}}. \quad (13)$$

Through the same modeling procedure for  $\Pi_{i\theta}$ , a model of  $\phi_{i\theta}$  can also be obtained as:

$$\phi_{i\theta} = \begin{cases} C_{\phi} f_{\phi 1} f_{\phi 2} C_p \sqrt{(Re_t)} \frac{\sqrt{(Pr)}}{\sqrt{(R)}} \sqrt{\left(\frac{k}{2\overline{u_{i0}^2}}\right) \frac{\varepsilon}{k} \overline{u_i \theta}} & \text{(Model 1)} \\ \frac{\sqrt{3}}{2} C_{\phi} f_{\phi 1} f_{\phi 2} C_p \sqrt{(Re_t)} \frac{\sqrt{(Pr)}}{\sqrt{(R)}} \frac{\varepsilon}{k} \overline{u_i \theta} & \text{(Model 2)} \end{cases} \quad (14)$$

where a relationship  $\sqrt{((\partial\theta/\partial x_i)^2)} = \sqrt{(\varepsilon_{\theta}/\alpha)}$  is utilized. The difference between equations (11) and (14) originates from the choice of the length scales that are used for estimating the derivatives of fluctuation quantities, i.e.  $\lambda/\lambda_{\theta} \propto \sqrt{(Pr/R)}$  ( $\lambda_{\theta}$  is the Taylor microscale of scalar fluctuations). Therefore, if the spectra of turbulent energy and scalar variance do not overlap at a high wave-number range ( $\lambda \neq \lambda_{\theta}$ ), and also if the functions  $f_{\Pi 2}$  and  $f_{\phi 2}$  are of order one, equations (11) and (14) may give greatly different results. In order for the model to satisfy the condition of (13), the correlation coefficients of  $\Pi_{i\theta}$  and  $\phi_{i\theta}$  must decrease accordingly. Thus  $f_{\Pi 2}$  and  $f_{\phi 2}$  must satisfy at least the following inequalities:

$$f_{\Pi 2} \leq \min \left[ 1, \frac{C_{\phi}}{C_{\Pi}} \frac{\sqrt{(Pr)}}{\sqrt{(R)}} \right] \quad (15)$$

$$f_{\phi 2} \leq \min \left[ 1, \frac{C_{\Pi}}{C_{\phi}} \frac{\sqrt{(R)}}{\sqrt{(Pr)}} \right]. \quad (16)$$

The physical meaning of these inequalities is that the derivative of a fluctuating quantity which appears in the correlation should be estimated at least at a scale larger than both  $\lambda$  and  $\lambda_{\theta}$  ( $\partial/\partial x_i \leq O(\min[1/\lambda, 1/\lambda_{\theta}])$ ). In other words, the derivative of a fluctuating quantity with the length scale smaller than either of  $\lambda$  or  $\lambda_{\theta}$  cannot correlate well with other fluctuations such as  $\theta$  or  $p$ .

We now return to the transport equation of  $\overline{u_i \theta}$ . If a local equilibrium condition holds, the transport equation of  $\overline{u_i \theta}$  can be written as:

$$0 = P_{i\theta} + \Pi_{i\theta} - \varepsilon_{i\theta}. \quad (17)$$

With the assumptions that  $\overline{u_i \theta} \sim \sqrt{(kk_{\theta})}$ ,  $\overline{u_i u_j} \sim k$ ,  $\partial U_i/\partial x_j \sim \varepsilon/k$  and  $\partial \Theta/\partial x_i \leq C_R \varepsilon_{\theta}/\sqrt{(kk_{\theta})}$ , the order of magnitude of each term can be estimated as:

$$P_{i\theta} = O\left(\frac{\varepsilon}{k} \sqrt{(kk_{\theta})} \left[\frac{C_R}{R} + 1\right]\right) \quad (18)$$

$$\Pi_{i\theta} = O\left(\frac{\varepsilon}{k} \sqrt{(kk_{\theta})} [\sqrt{(Re_t)} f_{\Pi 1} f_{\Pi 2}]\right) \quad (19)$$

$$\varepsilon_{i\theta} = O\left(\frac{\varepsilon}{k} \sqrt{(kk_{\theta})} \left[\frac{1 + Pr}{\sqrt{(Pr)}\sqrt{(R)}} f_{\varepsilon 1} f_{\varepsilon 2}\right]\right). \quad (20)$$

In order to restrict  $\Pi_{i\theta}$  and  $\varepsilon_{i\theta}$  not to exceed  $P_{i\theta}$ , the following inequalities must be satisfied:

$$\sqrt{(Re_t)} f_{\Pi 1} f_{\Pi 2} \leq c' \left(\frac{C_R}{R} + 1\right) \quad (21)$$

$$\frac{1 + Pr}{\sqrt{(Pr)}\sqrt{(R)}} f_{\varepsilon 1} f_{\varepsilon 2} \leq c'' \left(\frac{C_R}{R} + 1\right). \quad (22)$$

The coefficients  $c'$  and  $c''$  should be of  $O(1)$ . The functions  $f_{\Pi 1}$ ,  $f_{\Pi 2}$ ,  $f_{\varepsilon 1}$  and  $f_{\varepsilon 2}$  are now chosen so that relationships of (15), (21) and (22) should hold at any state, e.g.  $Pr \rightarrow 0$  or  $\infty$ , and  $Re_t \rightarrow 0$  or  $\infty$ . As mentioned earlier, functions  $f_{\Pi 1}$  and  $f_{\varepsilon 1}$  are chosen so as to express the effect of broadening of the spectra, while functions  $f_{\Pi 2}$  and  $f_{\varepsilon 2}$  must bear the effect of scale difference between scalar and velocity fields at high wave numbers. Finally, these functions are modeled as follows:

$$f_{\Pi 1} = 1 - \exp(-10r) \quad (23)$$

$$f_{\varepsilon 1} = 1 - \exp(-10r) \quad (24)$$

$$f_{\Pi 2} = \min \left[ 1, \frac{1}{1.2} \frac{\sqrt{(Pr)}}{\sqrt{(R)}} \right] \quad (25)$$

$$f_{\varepsilon 2} = \min \left[ 6 \frac{\sqrt{(Pr)}}{\sqrt{(R)}}, 1, \frac{\sqrt{(R)}}{\sqrt{(Pr)}} \right] \quad (26)$$

where  $r = (C_R/R+1)/(\sqrt{(Re_t)}f_{\Pi 2})$ . The constants in equations (23)–(26) are optimized by referring to the direct numerical simulation (DNS) and experimental results satisfactorily. It must be noted that, since function  $f_{e1}$  cannot be determined only from the condition of (22), it is assumed equal to  $f_{\Pi 1}$  in order to conform to a locally isotropic state, i.e.  $\varepsilon_{i\theta} \rightarrow 0$  if  $r \rightarrow 0$ .

The parameter  $\sqrt{(Pr/P)}$  that appears in  $f_{\Pi 2}$  and  $f_{e2}$  is the ratio between the Taylor microscales of velocity and scalar fluctuations,  $\lambda$  and  $\lambda_\theta$ . It can also be considered as the time scale ratio between the velocity and scalar fields at high wave-number regions, when the same velocity scale is used for conversion from length to time scales. On the other hand, the parameter  $r$  in  $f_{\Pi 1}$  and  $f_{e1}$  can be interpreted as the ratio of the two characteristic time scales, if rewriting it as:

$$r = \frac{\max \left[ \sqrt{\left(\frac{\nu}{\varepsilon}\right)} 1.2 \sqrt{\left(\frac{\nu}{\varepsilon}\right)} \sqrt{\left(\frac{R}{Pr}\right)} \right]}{1 / \left( \frac{1}{k/\varepsilon} + \frac{C_R}{k_\theta/\varepsilon_\theta} \right)}. \quad (27)$$

The numerator denotes the choice of the larger between the two fine time scales, while the denominator the smaller between the two large time scales. Thus, the rates of decrease of the correlation coefficients are proportional to these time and length scale ratios,  $\sqrt{(Pr/R)}$  and  $r$ . With equations (23)–(26), the proper characteristic time scales are automatically selected when the present model is applied to a flow which involves time scales.

As previously noted, the coefficient  $C_p$  relates the pressure fluctuation to the turbulent kinetic energy  $k$ . Since we didn't deal so far the so-called slow and rapid parts of  $\Pi_{i\theta}$  separately,  $C_p$  must represent the effects of these processes. For example, the DNS data [20] show that  $C_p$  takes a larger value in the presence of mean velocity gradient, while it decreases remarkably near a wall since  $\sqrt{(p^2)}$  does not show a strong peak as  $k$ . In order to account for these features,  $C_p$  is expressed as a function of  $P/\varepsilon$  and the flatness parameter  $A$  as:

$$C_p = \sqrt{(A)} \left( 0.8 + 0.3 \frac{P}{\varepsilon} \right) \quad (28)$$

where  $A = 1 - 9/8(a_{ij}a_{ij} - a_{ij}a_{jk}a_{ki})$ ,  $a_{ij} = (\overline{u_i u_j})/k - 2/3\delta_{ij}$  and  $P = -\overline{u_i \mu_j} \partial U_i / \partial x_j$ .

An *a priori* test of equations (11) and (12) with the aid of DNS and experimental data in several fundamental flows is described below. Here, the sum of scalar-pressure gradient correlation and dissipation terms is compared with:

$$\Pi_{1\theta} - \varepsilon_{1\theta} = -C_{(1)} \frac{\varepsilon}{k} \overline{u_1 \theta} \quad (29)$$

$$\Pi_{2\theta} - \varepsilon_{2\theta} = -C_{(2)} \frac{\varepsilon}{k} \overline{u_2 \theta} \quad (30)$$

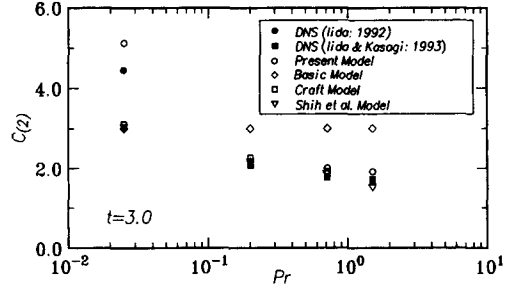


Fig. 1. Dependence of the model constant of  $\Pi_{i\theta} - \varepsilon_{i\theta}$  on the Prandtl number in isotropic turbulence with a constant mean scalar gradient.

$$\Pi_{3\theta} - \varepsilon_{3\theta} = -C_{(3)} \frac{\varepsilon}{k} \overline{u_3 \theta} \quad (31)$$

where the model constant  $C_{(i)}$  is given by the present model as follows:

$$C_{(i)} = 0.264 f_{\Pi 1} f_{\Pi 2} \sqrt{(A)} \left( 0.8 + 0.3 \frac{P}{\varepsilon} \right) \sqrt{(Re_t)} \sqrt{\left( \frac{k}{2u_{(i)}^2} \right)} + 0.8 f_{e1} f_{e2} \frac{1 + Pr}{2\sqrt{(Pr)}\sqrt{(R)}} \quad (\text{Model 1}) \quad (32)$$

$$C_{(i)} = 0.264 \frac{\sqrt{3}}{2} f_{\Pi 1} f_{\Pi 2} \sqrt{(A)} \left( 0.8 + 0.3 \frac{P}{\varepsilon} \right) \sqrt{(Re_t)} + 0.8 f_{e1} f_{e2} \frac{1 + Pr}{2\sqrt{(Pr)}\sqrt{(R)}} \quad (\text{Model 2}). \quad (33)$$

The DNS or experimental data are directly substituted into the model expression [equations (32) and (33)] and compared with the results obtained from the definition [ $\Pi_{i\theta}$  and  $\varepsilon_{i\theta}$  in equations (29)–(31)].

First, the model is tested in isotropic turbulence with a constant mean scalar gradient ( $\partial \Theta / \partial x_2 = \text{const.}$ ). In isotropic turbulence,  $C_{(i)}$  corresponds to the model constant of the slow term. Note that both Models 1 and 2 take exactly the same form in this flow. In Fig. 1, the Prandtl number dependence of  $C_{(2)}$  is shown. The predictions of Craft [5] and Shih *et al.* [21] are also included for comparison. The DNS data [22, 23] reveal that the value of this constant increase in low  $Pr$  and asymptotes to a value around 1.7 at high  $Pr$ . This tendency is well captured by the present model. The effect of the turbulent Reynolds number is shown in Fig. 2. The value of  $C_{(2)}$  increases with  $Re_t$ , as indicated by the experimental data of Maekawa and Kobayashi [24]. In their experiment, the ratio of the grid diameter  $d$  to the mesh size  $M$  is changed in order to produce four different Reynolds number flows; e.g.  $Re_t^{\text{init}} \approx 100$  for  $d/M = 0.15$  and  $Re_t^{\text{init}} \approx 330$  for  $d/M = 0.30$ . This Reynolds number dependence is predicted only by the present model. Finally, the effect of time scale ratio is shown in Fig. 3. The experimental data of Sirivatt and Warhaft [25] show that  $C_{(2)}$  slightly decreases as  $R$  increases. Note that the closed symbols denote experiments performed

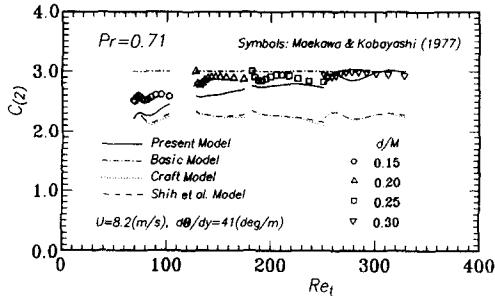


Fig. 2. Dependence of the model constant of  $\Pi_{i0} - \epsilon_{i0}$  on the turbulent Reynolds number in isotropic turbulence with a constant mean scalar gradient.

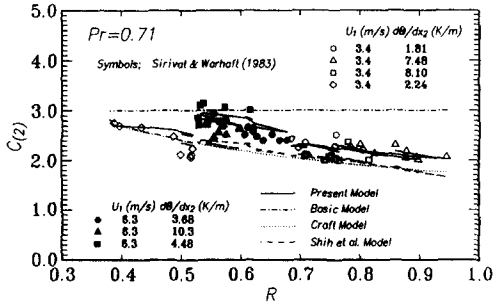


Fig. 3. Dependence of the model constant of  $\Pi_{i0} - \epsilon_{i0}$  on the time scale ratio in isotropic turbulence with a constant mean scalar gradient.

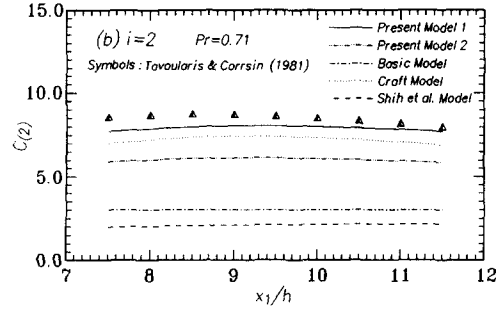
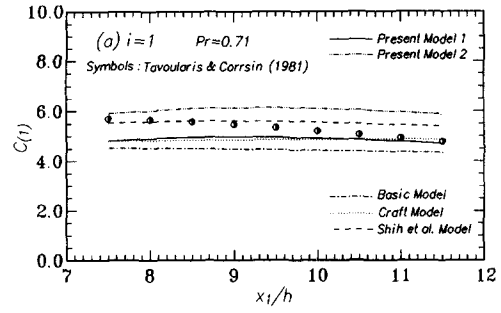


Fig. 4. Dependence of the model constant  $\Pi_{i0} - \epsilon_{i0}$  on the mean shear rate in homogeneous shear flow with constant mean scalar gradients.

at a slightly higher Reynolds number than the cases denoted by the open symbols. The Reynolds number effect is well predicted again by the present model.

Secondly, the experimental data of homogeneous shear flow [26] is utilized. In this case,  $C_{(1)}$  as well as  $C_{(2)}$  can be defined. As seen in Fig. 4, the value of  $C_{(2)}$  is about 1.7 times larger than that of  $C_{(1)}$ , and this is the major reason why most of the conventional models fail in this flow. Jones and Musonge [15] and also Craft [5] introduced a term which contains the mean scalar gradient into the modeled pressure–scalar gradient correlation term to overcome this problem. The present Model 1 can also express this strongly anisotropic feature by introducing the correlation coefficient of the turbulent scalar flux as a variable.

2.2. Modeling  $T_{i0}$  and  $V_{i0}$

The generalized gradient diffusion hypothesis (GGDH) is used to model the turbulent diffusion term  $T_{i0}$ :

$$T_{i0} = \frac{\partial}{\partial x_k} \left( C_{01} f_R \frac{k}{\epsilon} u_i u_k \frac{\partial u_i \theta}{\partial x_j} \right) \quad (34)$$

where,  $f_R$  is a function of  $R$  which is derived from the eddy diffusivity for a local equilibrium flow as:

$$f_R = \frac{2}{\left( \frac{C_R}{R} + 1 \right)}. \quad (35)$$

This function takes the smaller of  $k/\epsilon$  and  $k_0/\epsilon_0$  as the characteristic time scale that appears in  $T_{i0}$ .

The molecular diffusion term  $V_{i0}$  also needs to be modeled. In the present study, the following simple model is adopted:

$$V_{i0} = \frac{(v + \alpha)}{2} \frac{\partial^2 u_i \theta}{\partial x_k^2}. \quad (36)$$

2.3. Modeling  $k_0$  and  $\epsilon_0$  equations

In order to calculate the scalar invariance and scalar time scale, the equations of  $k_0$  and  $\epsilon_0$  must be solved. The transport equation of the scalar variance  $k_0 = \overline{\theta^2}/2$  can be written as:

$$\frac{Dk_0}{Dt} = \underbrace{\alpha \frac{\partial^2 k_0}{\partial x_i^2}}_{V_0} - \underbrace{\frac{\partial}{\partial x_i} u_i \theta^2}_{T_0} - \underbrace{u_i \theta \frac{\partial \Theta}{\partial x_i}}_{P_0} - \underbrace{\frac{\partial \theta}{\partial x_i} \frac{\partial \theta}{\partial x_i}}_{\epsilon_0}. \quad (37)$$

The turbulent diffusion term  $T_0$  and the dissipation term  $\epsilon_0$  are the unknown terms in equation (37). For  $T_0$ , a GGDH model is adopted:

$$T_0 = \frac{\partial}{\partial x_k} \left( C_{02} f_R \frac{k}{\epsilon} u_j u_k \frac{\partial k_0}{\partial x_j} \right). \quad (38)$$

The dissipation term  $\epsilon_0$  is given from the following modeled equation:

Table 1. Model constants

$C_{\Pi}$	$C_{\epsilon}$	$C_R$	$C_{\theta 1}, C_{\theta 2}, C_{\theta 3}$	$C_{P1}$	$C_{P2}$	$C_{D1}$	$C_{D2}$
-0.264	0.8	0.7	0.3	0.8	0.3	1.0	0.3

$$\frac{D\epsilon_{\theta}}{Dt} = \alpha \frac{\partial^2 \epsilon_{\theta}}{\partial x_i^2} + T_{\epsilon\theta} + C_{P1} \frac{P_{\theta}}{k_{\theta}} \epsilon_{\theta} + C_{P2} \frac{P}{k} \epsilon_{\theta} - C_{D1} \frac{\epsilon_{\theta}}{k_{\theta}} \epsilon_{\theta} - C_{D2} \frac{\epsilon}{k} \epsilon_{\theta}. \quad (39)$$

The turbulent diffusion term  $T_{\epsilon\theta}$  is modeled in the same manner as  $T_{\theta}$  and  $T_{\theta}$ :

$$T_{\epsilon\theta} = \frac{\partial}{\partial x_k} \left( C_{\theta 3} f_R \frac{k}{\epsilon} u_j u_k \frac{\partial \epsilon_{\theta}}{\partial x_j} \right). \quad (40)$$

The values of the model constants in the turbulent diffusion terms (34), (38) and (40) are set as  $C_{\theta 1} = C_{\theta 2} = C_{\theta 3} = 0.3$ , since these values give good results in channel flows. The model constants in equation (39) are optimized so that it gives good results in isotropic turbulence, homogeneous shear and channel flows. The values of the model constants are summarized in Table 1.

### 3. MODEL TESTING IN BASIC FLOWS

The model described in the previous section is tested in several fundamental flows.† The velocity field variables (i.e.  $U_i$ ,  $\overline{u_i u_j}$  and  $\epsilon$ ) are supplied from the DNS and experimental data, and the differential equations only for  $\Theta$ ,  $\overline{u_i \theta}$ ,  $k_{\theta}$  and  $\epsilon_{\theta}$  are solved, so that any failure in the results can be attributed to the scalar field modeling.

#### 3.1. Homogeneous shear flow

The DNS of Rogers *et al.* [27] are utilized. In their simulation, the constant mean scalar gradient is imposed in three orthogonal directions; cases 1, 2 and 3 correspond the mean scalar gradient in the  $x_1$ ,  $x_2$  and  $x_3$  directions, respectively. Most turbulence models have been tested and qualified against the case in which the mean scalar gradient is aligned with the mean velocity gradient. Hence, it is important to study how those models perform in the case when the scalar gradient exists in other directions. The model predictions for the three cases are shown in Fig. 5. The present model and the Basic model give fairly good results in all cases, while other recent complex models achieve poorly, especially in case 1. This implies that the additional terms in the complex models do possess a possibility of giving erroneous results in the case

† The results in the flows which were already utilized in the *a priori* test in Section 2 (see Figs 1–4) will not be shown here. However, it is confirmed that the present model gives good results in those flows.

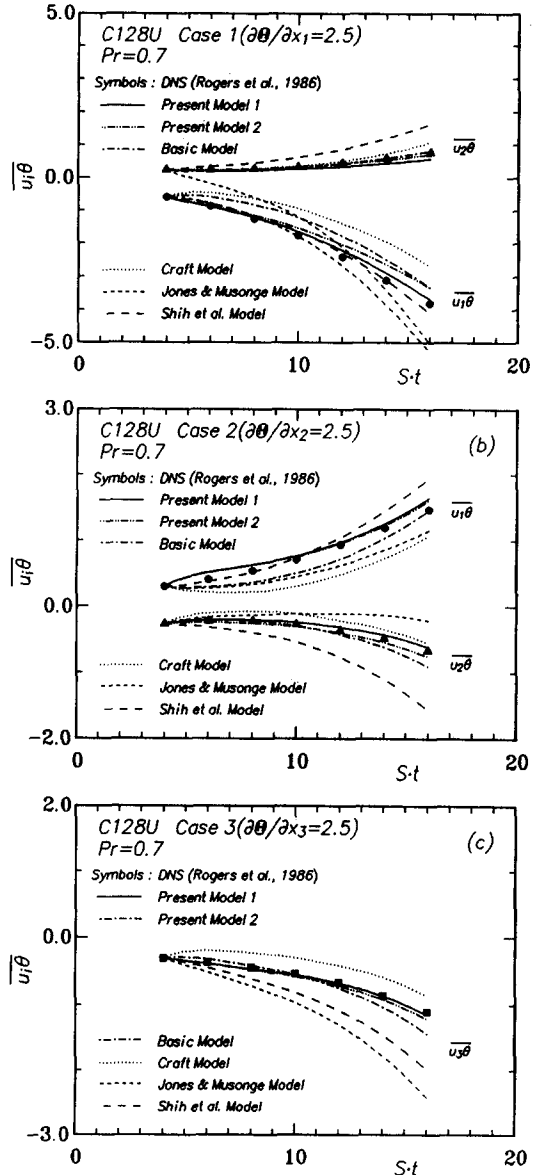


Fig. 5. Time development of turbulent scalar flux in homogeneous shear flow. (a) Case 1 ( $\partial\Theta/\partial x_1 = \text{const.}$ ), (b) Case 2 ( $\partial\Theta/\partial x_2 = \text{const.}$ ), (c) Case 3 ( $\partial\Theta/\partial x_3 = \text{const.}$ ).

where they have not been tested, while simpler models seem not to fail seriously.

#### 3.2. Fully developed channel flow

The model proposed should be modified for its application to the near-wall sublayer. To do this, a difficulty exists in the prediction of scalar transfer in high Prandtl number fluids as described in the following.

In the present study, the scalar fluctuation is assumed to be zero at the wall. This assumption is generally valid in an air flow (see Kasagi *et al.* [28]). Then the wall limiting value of  $R$  is equal to  $Pr$ :

$$R = Pr \quad \text{at } y = 0 \quad (41)$$

where  $y$  is the distance from the wall. Also,  $\lambda_\theta$  becomes of the same order as  $\lambda$ . The local Reynolds number is effectively small ( $r \gg 1$ ) in this region, and hence all the damping functions can be estimated as  $f_{\Pi 1} \sim f_{\Pi 2} \sim f_{\varepsilon 1} \sim f_{\varepsilon 2} \sim 1$ . If we now assume that the gradients of mean scalar quantities should scale with  $\lambda_\theta$  or  $\lambda$  (i.e.  $\partial/\partial x_i \sim 1/\lambda_\theta \sim 1/\lambda$ ), the order of magnitude of the model terms such as equations (11), (12), (34) and (36) can be estimated as follows:

$$T_{i\theta} = O\left(\frac{\varepsilon}{k}\sqrt{(kk_\theta)}\sqrt{(Re_t)}\right) \quad (42)$$

$$V_{i\theta} = O\left(\frac{\varepsilon}{k}\sqrt{(kk_\theta)}\left[\frac{1}{Pr} + 1\right]\right) \quad (43)$$

$$\Pi_{i\theta} = O\left(\frac{\varepsilon}{k}\sqrt{(kk_\theta)}\sqrt{(Re_t)}\right) \quad (44)$$

$$\varepsilon_{i\theta} = O\left(\frac{\varepsilon}{k}\sqrt{(kk_\theta)}\left[\frac{1}{Pr} + 1\right]\right). \quad (45)$$

However, in the vicinity of the wall (e.g.  $y^+ \leq 10$ ), the order of magnitude of the scalar flux production term  $P_{i\theta}$  cannot be estimated as in equation (18) when  $Pr \gg 1$ . The estimation  $\partial U_i/\partial x_j \sim C_S\sqrt{(\varepsilon/\nu)}$  should be used instead of  $\partial U_i/\partial x_j \sim \varepsilon/k$  since the viscous dissipation of mean kinetic energy  $\nu(\partial U_i/\partial x_j)^2$  is of the same order as  $\varepsilon$ . Then the order of magnitude of  $P_{i\theta}$  can be written as:

$$P_{i\theta} = O\left(\frac{\varepsilon}{k}\sqrt{(kk_\theta)}\left[\frac{C_R}{R} + C_S\sqrt{(Re_t)}\right]\right). \quad (46)$$

If the scalar flux equation is assumed to be at a local equilibrium state,  $V_{i\theta}$  and  $\varepsilon_{i\theta}$  cannot exceed  $P_{i\theta}$ . In order to satisfy this condition, functions  $f_{\varepsilon w}$  and  $f_{Vw}$  are introduced into the models of  $V_{i\theta}$  and  $\varepsilon_{i\theta}$ .

$$V_{i\theta} = \frac{(v+\alpha)}{2} \frac{\partial}{\partial x_k} \left[ f_{Vw} \frac{\partial u_i \theta}{\partial x_k} \right] \quad (47)$$

$$\varepsilon_{i\theta} = C_\varepsilon f_{\varepsilon 1} f_{\varepsilon 2} f_{\varepsilon w} \frac{1+Pr}{2\sqrt{(Pr)}\sqrt{(R)}} \frac{\varepsilon}{k} \overline{u_i \theta}. \quad (48)$$

In the present study,  $f_{\varepsilon w}$  and  $f_{Vw}$  are given in a simple form as:

$$f_{\varepsilon w} = f_{Vw} = \min\left[1, \frac{C_R}{R} + C_S\sqrt{(Re_t)}\right] \quad (49)$$

where the constant  $C_S$  is given a value of 0.1. Note that this modification only works for high Prandtl number flows, and it is not necessary for other cases (e.g.,  $Pr < O(10^1)$ ).

It is also important to satisfy the wall limiting behavior [29]. The terms that balance at the lowest order of  $y$  at the wall are  $V_{i\theta}$ ,  $\Pi_{i\theta}$  and  $\varepsilon_{i\theta}$ , and each of them requires some additional modification. In this study, the models proposed in the previous section are bridged with the expressions that satisfy the wall limiting behavior:

$$V_{i\theta} = \frac{\partial}{\partial x_k} \left[ \left\{ \frac{(v+\alpha)}{2} \frac{\partial u_i \theta}{\partial x_k} + n_i n_j \frac{(v-\alpha)}{6} \frac{\partial u_j \theta}{\partial x_k} \right\} f_w + \left\{ \frac{(v+\alpha)}{2} \frac{\partial u_i \theta}{\partial x_k} \right\} (1-f_w) \right] \quad (50)$$

$$\Pi_{i\theta} = -\frac{\varepsilon}{k} \overline{u_k \theta} n_k n_i f_w + C_{\Pi} f_{\Pi 1} f_{\Pi 2} C_p \sqrt{(Re_t)} \sqrt{\left(\frac{k}{2u_{i\theta}^2}\right)} \frac{\varepsilon}{k} \overline{u_i \theta} \quad (51)$$

$$\varepsilon_{i\theta} = \left\{ \frac{1+Pr}{2Pr} \frac{\varepsilon}{k} \overline{u_i \theta} + \frac{1+Pr}{2Pr} \frac{\varepsilon}{k} \overline{u_k \theta} n_k n_i \right\} f_w + \left\{ C_\varepsilon f_{\varepsilon 1} f_{\varepsilon 2} \frac{1+Pr}{2\sqrt{(Pr)}\sqrt{(R)}} \frac{\varepsilon}{k} \overline{u_i \theta} \right\} (1-f_w) \quad (52)$$

where  $n_i$  is the wall normal unit vector and  $f_w$  is a function that changes from unity to zero as it moves away from the wall. Note that only Model 1 of  $\Pi_{i\theta}$  is used here since it can reproduce large anisotropy of scalar fluxes without any *ad hoc* wall reflection modeling. Although its form violates vectorial invariance, Model 1 shows great improvement in strongly sheared turbulence where the turbulence anisotropy is very large, if a coordinate axis is set parallel to the mean flow direction. Its simplicity is so attractive that it is adopted as the  $\Pi_{i\theta}$  model for wall flows in this study. The function  $f_w$  is chosen as follows:

$$f_w = \exp[-C_{w1}\sqrt{(A)}] \quad (53)$$

where  $C_{w1} = \max[4, 0.6Pr^{3/4}]$ .

Referring to Kawamura and Hada [30], the  $\tilde{\varepsilon}_\theta (= \varepsilon_\theta - 2\alpha(\max[\partial\sqrt{(k_\theta)}/\partial y, 0])^2)$  equation is solved instead of  $\varepsilon_\theta$  equation for the sake of numerical stability:

$$\frac{D\tilde{\varepsilon}_\theta}{Dt} = \alpha \frac{\partial^2 \tilde{\varepsilon}_\theta}{\partial x_i^2} + \frac{\partial}{\partial x_k} \left( C_{\theta 3} f_R \frac{k}{\varepsilon} \overline{u_j u_k} \frac{\partial \tilde{\varepsilon}_\theta}{\partial x_j} \right) + C_{P1} \frac{P_\theta}{k_\theta} \tilde{\varepsilon}_\theta + C_{P2} \frac{P}{k} \tilde{\varepsilon}_\theta - C_{D1} \frac{\tilde{\varepsilon}_\theta}{k_\theta} \tilde{\varepsilon}_\theta - C_{D2} \frac{\tilde{\varepsilon}}{k} \tilde{\varepsilon}_\theta + E - \frac{\tilde{\varepsilon}_\theta \tilde{\varepsilon}_\theta}{k_\theta} \quad (54)$$

where  $\tilde{\varepsilon} = \varepsilon - 2\nu(\partial\sqrt{(k)}/\partial y)^2$ ,  $\tilde{\varepsilon}_\theta = 2\alpha(\partial\sqrt{(k_\theta)}/\partial y)^2$ ,  $E = 2\alpha C_{w2}(k_\theta/\varepsilon_\theta)v^2(\partial^2\Theta/\partial y^2)^2$  and  $C_{w2} = \max[0.1, 0.35 - 0.21Pr]^\dagger$ .

Then the model is applied to fully developed turbulent channel flows. The DNS data of Kasagi *et al.* [32], Kasagi and Ohtsubo [33] and Kim and Moin

<sup>†</sup> The authors apologize for typos in the definitions of  $E$  and  $C_{w2}$  in the previous paper presented at the 9th Symposium of Turbulent Shear Flows [31].



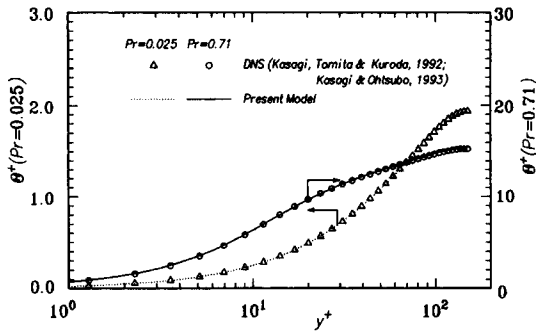


Fig. 6. Mean scalar profiles in fully developed turbulent channel flow.

[34] are used. The mean scalar profiles at  $Pr = 0.025$  and  $0.71$  are shown in Fig. 6. It can be said that the mean scalar profiles are well predicted in both cases. In Fig. 7, comparison is made with the DNS data at three different Prandtl numbers, i.e.  $Pr = 0.025, 0.71$  and  $2.0$ . The ratio of the two components of the scalar flux  $-\overline{u_i \theta} / u_2 \theta$  changes drastically with increasing the Prandtl number; it becomes greater than 10 near the wall at  $Pr = 2.0$ . The present model captures even quantitatively well this strongly anisotropic feature of the scalar field. It is surprising that these results have been obtained with a simple  $\Pi_{i\theta}$  model in which no wall reflection effect is taken into account. The predicted budget profiles of  $\overline{u_i \theta}$  are compared with the DNS data in Fig. 8. In the budget of  $Pr = 0.025$ , the scalar-pressure gradient correlation term does not make any appreciable contribution and the dissipation balances with the production. For  $Pr = 0.71$ , however, the scalar-pressure gradient correlation term almost balances with the production term. This tendency is successfully predicted by the present model.

Finally, the Nusselt number  $Nu$  is plotted against a wide range of Prandtl number ( $2.5 \times 10^{-2} < Pr < 10^4$ ) for  $Re_\tau = 150$  in Fig. 9. The empirical function of Sleicher and Rouse [35] for pipe flows is also plotted for comparison. It is known that the Nusselt number is nearly proportional to  $Pr^{1/3}$  at high Prandtl numbers, and this Prandtl number dependence is well predicted.

4. CONCLUSIONS

A second-moment closure is proposed for predicting turbulent scalar transport in various Prandtl number fluids. The correlation coefficients of the scalar-pressure gradient correlation and also of the dissipation terms are defined in the turbulent scalar flux equation. It is argued that these coefficients must decrease when the fluctuations arise at different scales and that the rate of decrease is to be proportional to the ratios between time scales and Taylor microscales involved. As a result, the present model coefficients are expressed as functions of the turbulent Reynolds

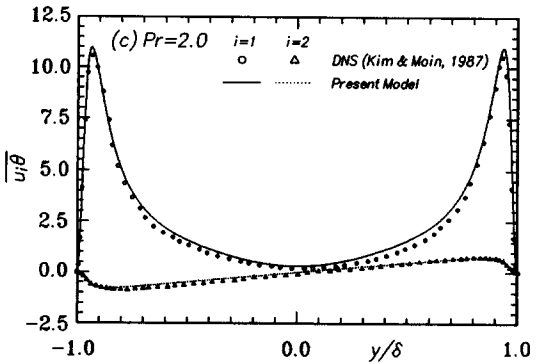
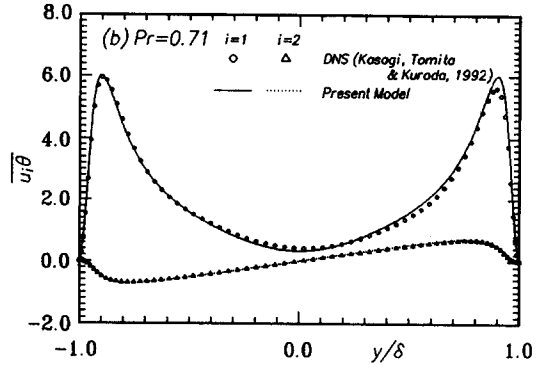
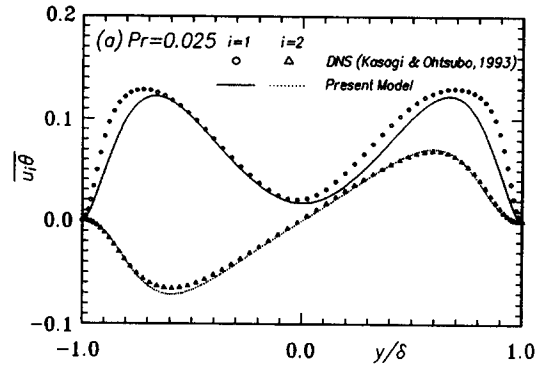


Fig. 7. Turbulent scalar flux profile in fully developed turbulent channel flow. (a)  $Pr = 0.025$ , (b)  $Pr = 0.71$ , (c)  $Pr = 2.0$ .

number  $Re_\tau$ , the Prandtl number  $Pr$  and the time scale ratio  $R$ .

The present model predicts well the turbulent scalar fluxes in isotropic turbulence with a constant mean scalar gradient, where the model constants show large variations over wide  $Pr$  and  $Re_\tau$  ranges. The scalar-pressure gradient model, especially Model 1 given by equation (11), predicts well the large anisotropy of turbulent scalar flux in wall turbulence. Although Model 1 does not assume vectorial invariance, it shows great improvement in simple shear flows provided that one of the coordinate axis is defined in alignment with the main flow direction. Model 1 must be used with care in this respect.

Acknowledgements—The authors acknowledge the financial

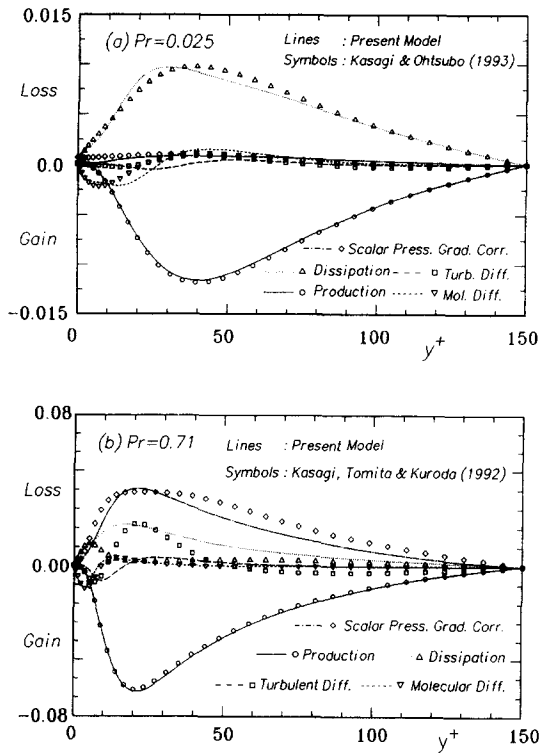


Fig. 8. Budgets of  $\overline{u_s \theta}$  in fully developed turbulent channel flow. (a)  $Pr = 0.025$ , (b)  $Pr = 0.71$ .

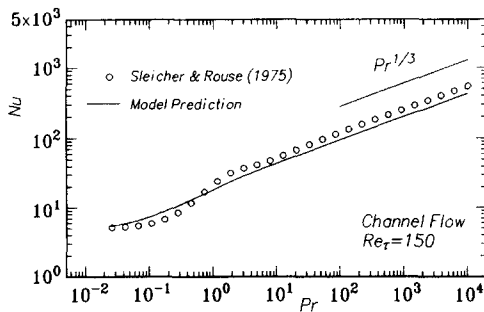


Fig. 9. Prandtl number dependence of Nusselt number in fully developed turbulent channel flow.

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